

QUESTION 1.

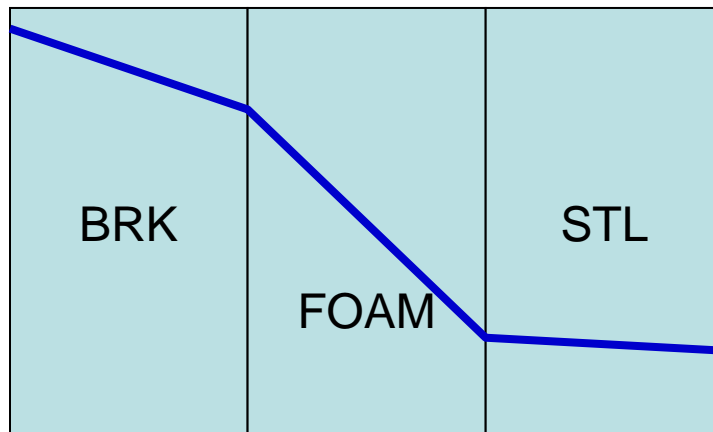
Write the equation for internal energy change for subcooled water entering a heat exchanger at T_1 and leaving as a superheated vapor at T_2 .

$$\Delta U = \dot{m} c_{p,\text{liq}} (T_{\text{sat}} - T_1) + \dot{m} h_{\text{fg}} + \dot{m} c_{p,\text{vap}} (T_2 - T_{\text{sat}})$$

QUESTION 2.

For a composite wall made of equal thicknesses of:
BRICK | POLYMER FOAM | STAINLESS STEEL

Draw an estimate of the steady state temperature profile assuming the brick side is hotter.

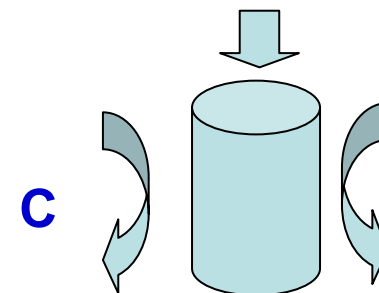
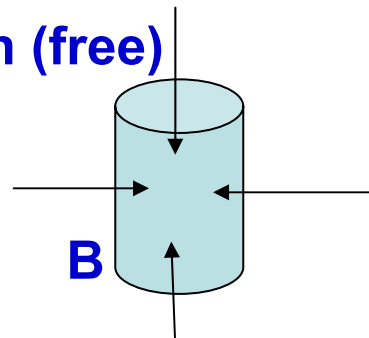


QUESTION 3.

3-part question:

- A. For a cold soda can sitting on a table, which mode(s) of heat transfer are most important?
- B. Draw the can with arrows showing the direction of heat transfer.
- C. Use a different color to show the direction of any fluid flow in the problem.

A. conduction & convection (free)



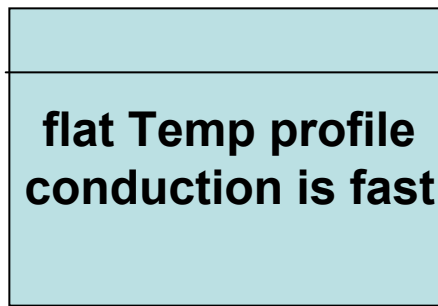
QUESTION 4.

Write the equation for the Biot Number.

What does the temperature profile look like in a solid if $Bi = 0.0001$?

$$Bi = hL_c/k_{\text{solid}}$$

T



QUESTION 5.

**Write the Stefan-Boltzmann equation.
What are the units of the
Stefan-Boltzmann constant?**

$$q = \epsilon \sigma (T_s^4 - T_{sur}^4)$$

$$\text{units} = \text{W/m}^2\text{-K}^4$$

QUESTION 6.

**Write Newton's Law of Cooling for flow through a large tube bundle.
What temperature do you use to find fluid properties?**

$$q = hA(T_s - T_{\text{mean}})$$

$$\text{where } T_{\text{mean}} = (T_{\text{in}} + T_{\text{out}}) / 2$$

Fluid properties at T_{mean}

QUESTION 7.

The surface of a pipe is held constant @ 125 °C. Glycerin enters the pipe at 25 °C and exits at 35 °C.

A. What temperature do you use to look up fluid properties? **30 °C**

B. What is the ΔT associated with internal energy change? **35 - 25 = 10 °C**

C. What is the temperature driving force for heat transfer?

$$\begin{aligned}\Delta T_{lm} &= (125-25) - (125-35) / \ln (100/90) \\ &= 94.9 \text{ °C}\end{aligned}$$

QUESTION 8.

What are the 5 terms that make up the total resistance in a heat exchanger?

h_i = internal (tubeside) convective heat transfer coefficient

$R_{f,i}$ = internal fouling factor

k_w = conduction term through wall $\ln(D_o/D_i)/2\pi Lk_w$

h_o = external (shellside) convective heat transfer coefficient

$R_{f,o}$ = external (shellside) fouling factor

QUESTION 9.

Given a shell & tube heat exchanger with a low shell-side Reynolds number:

List 2 changes you can make to increase Re.

possibilities: decrease baffle pitch, decrease shell diameter, increase # of tubes, decrease tube pitch

List two changes that will increase Re if Re is low on the tubeside.

possibilities: decrease tube diameter, decrease number of tubes, use a rough surface in pipes

QUESTION 10.

Write Fourier's Law for heat conduction in the x-direction.

What are the English units for thermal conductivity?

$$q = -k \, dT/dx$$

k is in Btu/h-ft-°F (W/m-K)

QUESTION 11.

LIST THREE OF THE FOUR HEAT TRANSFER REGIMES FOUND IN POOL BOILING.

**Free Convection
Nucleate
Transition
Film**

QUESTION 12.

What Reynolds number marks the transition from laminar to turbulent flow for:

- A. Flow over a flat plate
- B. Flow through a pipe.

$$5 \times 10^5$$

$$\sim 2100-2300$$